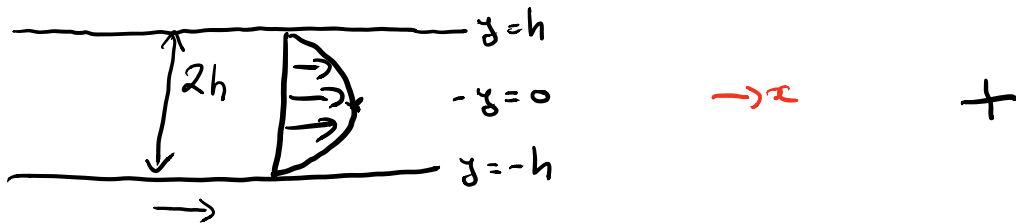


Poiseuille Flow (Pressure-driven flow between 2 plates)



Assumptions:

- 2 dimensional (x, y)
- Incompressible ($\rho = \text{const}$)
- Fully developed ($\frac{\partial}{\partial x} = 0$, except $\frac{\partial p}{\partial x}$)
- Steady State ($\frac{\partial}{\partial t} = 0$)

$$0 = \frac{\partial \rho}{\partial t} + \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} \Rightarrow \boxed{\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0}$$

$$\rho \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) = -\frac{\partial p}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right)$$

$$\frac{\partial v}{\partial y} = 0 \Rightarrow v = \text{constant} = 0, \text{ because } \boxed{v = 0} \text{ @ } y = \pm h$$

$$\boxed{\frac{\partial p}{\partial x} = \mu \frac{\partial^2 u}{\partial y^2}}$$

$$\int \frac{d^2 u}{dy^2} dy = \int \frac{1}{\mu} \frac{dp}{dx} dy$$

$$\int dy \rightarrow \frac{du}{dy} = \frac{1}{\mu} \frac{dp}{dx} y + C_1$$

$$u = \frac{1}{2\mu} \frac{dp}{dx} y^2 + C_1 y + C_2$$

$$u = 0 \text{ @ } y = \pm h \quad - 2 \text{ B.C. (No slip)}$$

$$\begin{aligned} \text{at } y=h \Rightarrow 0 &= \frac{1}{2\mu} \frac{dp}{dx} h^2 + C_1 h + C_2 \\ \text{AND} \\ \text{at } y=-h \Rightarrow 0 &= \frac{1}{2\mu} \frac{dp}{dx} h^2 - C_1 h + C_2 \end{aligned}$$

$$C_2 = -\frac{1}{2\mu} \frac{dp}{dx} h^2$$

$$u = \frac{1}{2\mu} \frac{dp}{dx} (y^2 - h^2)$$

$$\bar{u} = \frac{1}{2h} \int_{-h}^h u \, dy = -\frac{h^2}{3\mu} \frac{\partial p}{\partial x}$$

$\frac{\partial p}{\partial x} < 0$
pressure drops from high to low

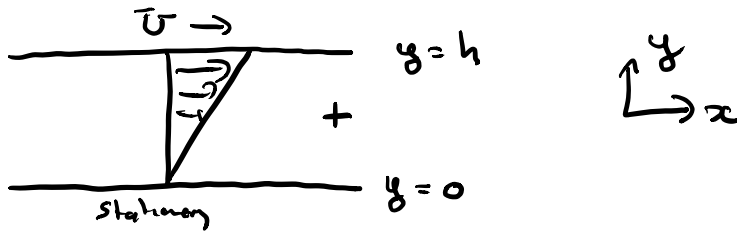
$$u_{max} = u|_{y=0} = \frac{1}{2\mu} \frac{\partial p}{\partial x} (-h^2)$$

$$\frac{u_{max}}{\bar{u}} = 3/2$$

$$\tau = \mu \frac{du}{dy} = \frac{\mu}{2\mu} \frac{dp}{dx} (2y) = \frac{dp}{dx} y$$

$$\omega = \frac{1}{2} \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right) = -\frac{1}{2\mu} \frac{dp}{dx} y$$

Couette Flow (no pressure drop)



① Incompressible $\Rightarrow \frac{\delta u}{\delta x} + \frac{\delta v}{\delta y} + \frac{\delta w}{\delta z} = 0$

② 2d $\Rightarrow \frac{\delta u}{\delta x} + \frac{\delta v}{\delta y} = 0$

③ Fully developed ~~$\frac{\delta u}{\delta x} + \frac{\delta v}{\delta y} = 0$~~ $\Rightarrow v = \text{constant} = 0$
 because $v=0 @ y=0$

④ Steady State

$$\underbrace{\left(\frac{\delta u}{\delta t} \right)}_{\text{S.S.}} + \underbrace{u \frac{\delta u}{\delta x}}_{\text{F.D.}} + \underbrace{v \frac{\delta u}{\delta y}}_{v=0} + \underbrace{w \frac{\delta u}{\delta z}}_{\text{2D}} = \underbrace{-\frac{\delta p}{\delta x}}_{0 \text{ (no pressure drop)}} + \underbrace{\mu \left(\frac{\delta^2 u}{\delta x^2} + \frac{\delta^2 u}{\delta y^2} + \frac{\delta^2 u}{\delta z^2} \right)}_{\text{F.D.}} \quad \text{2D}$$

$$\boxed{\mu \frac{\delta^2 u}{\delta y^2} = 0}$$

$$\frac{d^2 u}{dy^2} = 0$$

$$\frac{du}{dy} = C_1$$

$$u = C_1 y + C_2$$

$$u = 0 @ y = 0 \rightarrow C_2 = 0$$

$$u = U @ y = h \rightarrow C_1 = \frac{U}{h}$$

$$u = U \frac{y}{h}$$

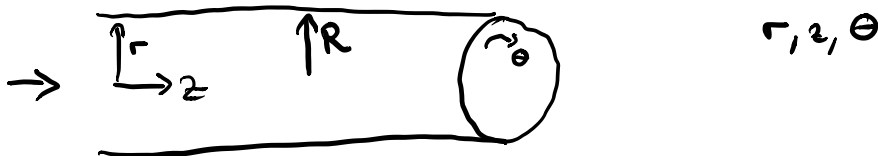
$$\bar{u} = \frac{1}{h} \int_0^h u dy = \frac{U}{2}$$

$$u_{\max} = U$$

$$\tau = \mu \frac{du}{dy} = \mu \frac{U}{h}$$

$$\omega = \frac{1}{2} \left(\frac{\delta v}{\delta x} - \frac{\delta u}{\delta y} \right) = -\frac{U}{2h}$$

Hagen - Poiseuille (Pressure Driven in a Pipe)



$$\text{Continuity} \Rightarrow \frac{\delta \rho}{\delta t} + \frac{1}{r} \left(\frac{\delta}{\delta r} (r \rho v_r) \right) + \frac{1}{r} \frac{\delta (\rho v_\theta)}{\delta \theta} + \frac{\delta (\rho v_z)}{\delta z} = 0$$

Assumption : ① Incompressible ; $\rho = \text{const}$

② 2d $\rightarrow r, z$

③ Fully developed $\rightarrow \frac{\delta}{\delta z} = 0$ (except p)

④ Steady State $\Rightarrow \delta/\delta t = 0$

Continuity $\Rightarrow \frac{1}{r} \left(\frac{\delta}{\delta r} (r v_r) \right) + \frac{\delta}{\delta z} v_z = 0$
F.D.

$$\frac{\delta}{\delta r} (r v_r) = 0$$

$$r v_r = \text{const} = 0$$

because $v_r = 0$ @ $r = R$

Momentum in z

$$\delta \left(\frac{\delta v_z}{\delta t} + v_r \frac{\delta v_z}{\delta r} + v_z \frac{\delta v_z}{\delta z} \right) = - \frac{\delta p}{\delta z}$$

S.S. $v_r = 0$ F.D.

$$+ \mu \left[\frac{1}{r} \frac{\delta}{\delta r} \left(r \frac{\delta v_z}{\delta r} \right) + \frac{\delta^2 v_z}{\delta z^2} \right]$$

F.D.

$$\frac{1}{\mu} \frac{\delta p}{\delta z} = \frac{1}{r} \frac{\delta}{\delta r} \left(r \frac{\delta v_z}{\delta r} \right)$$

$$\frac{r}{\mu} \frac{\delta p}{\delta z} = \frac{\delta}{\delta r} \left(r \frac{\delta v_z}{\delta r} \right)$$

$$\frac{r}{\mu} \frac{\delta p}{\delta z} dr = \delta \left(r \frac{\delta v_z}{\delta r} \right)$$

Integrate

$$\frac{r^2}{2\mu} \frac{dp}{dz} + C_1 = r \frac{\delta v_z}{\delta r}$$

$$\left(\frac{r}{2\mu} \frac{dp}{dz} + \frac{C_1}{r} \right) dr = \delta v_z$$

$$\frac{r^2}{4\mu} \frac{dp}{dz} + C_1 \ln(r) + C_2 = v_z$$

$$v_z = 0 \text{ @ } r = R$$

$$v_z \text{ is finite @ } r = 0 \Rightarrow C_1 = 0$$

$$C_2 = -\frac{R^2}{4\mu} \frac{dp}{dz}$$

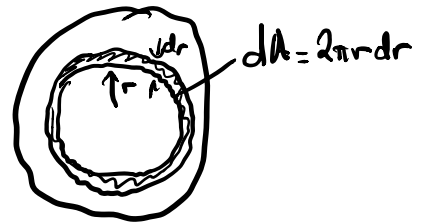
$$v_z = \frac{1}{4\mu} \frac{dp}{dz} (r^2 - R^2)$$

$$v_{z, \max} = v_z|_{r=0} = \frac{-1}{4\mu} \frac{dp}{dz} R^2$$

$$Q = \int_{A_R} v_z dA$$

$$= \int_0^R \frac{1}{4\mu} \frac{dp}{dz} (r^2 - R^2) 2\pi r dr$$

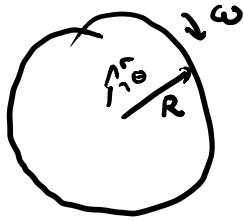
$$= \frac{-\pi}{8\mu} R^4 \frac{dp}{dz}$$



$$\bar{v} = \frac{Q}{\pi R^2} = \frac{-R^2}{8\mu} \frac{dp}{dz}$$

$$v_{\max} = 2\bar{v}$$

Flow Inside / Outside a rotating cylinder



r, θ, z

Inside

- Assume:
- ① 2d r, θ
 - ② Incompressible
 - ③ Steady $\delta/\delta t = 0$
 - ④ $\delta/\delta \theta = 0$ (axisymmetric)

Continuity $\Rightarrow \frac{1}{r} \frac{\delta}{\delta r} (r v_r) + \frac{1}{r} \frac{\delta v_\theta}{\delta \theta} = 0$
 $\delta/\delta \theta = 0$

$$\frac{\delta}{\delta r} (r v_r) = 0$$

$$r v_r = \text{const} = 0$$

because $v_r = 0$
 @ $r = R$

θ -momentum

$$\rho \left(\cancel{\frac{\delta v_\theta}{\delta t}} + v_r \cancel{\frac{\delta v_\theta}{\delta r}} + \frac{v_\theta}{r} \cancel{\frac{\delta v_\theta}{\delta \theta}} + \cancel{\frac{v_r v_\theta}{r}} \right)$$

$\delta - t$ $v_r = 0$ axisym $v_r = 0$

$$= \frac{1}{r} \frac{dp}{d\theta} + \mu \left[\frac{1}{r} \frac{\delta}{\delta r} \left(r \frac{\delta v_\theta}{\delta r} \right) \right]$$

$\delta - r$ v_θ

$\delta\theta = v$

$$\left[-\frac{1}{r^2} + \frac{1}{r^2} \frac{\delta^2 V_\theta}{\delta\theta^2} + \frac{2}{r^2} \frac{\delta V_\theta}{\delta\theta} \right]$$

F.D.
 $v_r = 0$

$$\cancel{\mu} \frac{1}{r} \frac{\delta}{\delta r} \left(r \frac{\delta V_\theta}{\delta r} \right) = \cancel{\mu} \frac{V_\theta}{r^2}$$

$$\boxed{r^2 \frac{\delta^2 V_\theta}{\delta r^2} + r \frac{\delta V_\theta}{\delta r} - V_\theta = 0}$$

$$\text{Euler eqn} \Rightarrow V_\theta = \frac{C_1}{r} + C_2 r$$

$$\text{Inside} \Rightarrow \boxed{V_\theta = \omega R} \text{ @ } r=R$$

$C_1 = 0$ because V_θ finite ($r=0$)

$$V_\theta = C_2 r$$

$$\Rightarrow C_2 = \omega$$

$$\therefore V_\theta = \omega r$$

$$\text{Outside} \Rightarrow V_\theta = \frac{C_1}{r} + C_2 r$$

$$\boxed{V_\theta = \omega R} \text{ @ } r=R$$

$C_2 = 0$ because V_θ is finite as $r \rightarrow \infty$

$$\omega R = \frac{C_1}{R}$$

$$C_1 = \omega R^2$$

$$\boxed{V_A = \frac{\omega R^2}{r}}$$



$$6.65 // \quad u = \frac{1}{2\mu} \frac{\delta p}{\delta x} (y^2 - h^2)$$

$$q = \int_{-h}^h u \, dy = -\frac{2h^3}{3\mu} \frac{\delta p}{\delta x}$$

$$h = 2.5 \text{ mm}$$

$$\mu = 0.4 \text{ N s m}^{-2}$$

$$\frac{\delta p}{\delta x} = -900 \text{ N m}^{-3}$$

$$q = 2.34 \times 10^{-5} \text{ m}^2 \text{ s}^{-1}$$

$$\begin{aligned} \tau &= \mu \frac{\delta u}{\delta y} = \mu \left(\frac{1}{2\mu} \frac{\delta p}{\delta x} (2y) \right) = \frac{\delta p}{\delta x} y \\ &= (-900) (2.5 \times 10^{-3}) \\ &= -2.25 \text{ N/m}^2 \end{aligned}$$

6.81 // Hagen - Poiseuille

$$\bar{v} = \frac{R^2}{8\mu} \left(-\frac{\delta p}{\delta x} \right)$$

$$R = 2 \text{ mm}$$

$$\mu = 0.002 \text{ N s/m}^2$$

Manometre $p_1 + \gamma \Delta h - \gamma_{\text{gas}} \Delta h = p_2$

$$\left(-\frac{\delta p}{\delta x} \right) = \frac{p_1 - p_2}{\Delta L} = \frac{(\gamma_{\text{gas}} - \gamma) \Delta h}{2}$$

$$- R^2 \Delta p = \dots \text{ m}^{-2} \dots$$

$$\bar{v} = \frac{8\mu}{\Delta l} \approx 1.1 \times 10^4 \text{ m/s}$$