

1) Dimensional Analysis of turkey cooking.

Cooking time t depends on: thermal diffusivity α
density ρ
mass m

Start by constructing a dimensional matrix

		$t = f(\alpha, \rho, m)$			
mass	M	0	0	1	1
length	L	0	2	3	0
time	T	1	-1	0	0

We have 4 variables.

$\begin{bmatrix} 0 & 1 & 1 \\ 2 & 3 & 0 \\ -1 & 0 & 0 \end{bmatrix}$ is a largest nonzero determinant submatrix, so
rank = 3

Buckingham Π theorem:

$$\# \text{ dimensionless groups} = \# \text{ vars} - \# \text{ rank of submatrix}$$

$$1 = 4 - 3$$

To find the dimensionless group, solve the system:

$$A x = b$$



1.) Continued

$$A = \begin{bmatrix} 0 & 1 & 1 \\ 2 & 3 & 0 \\ -1 & 0 & 0 \end{bmatrix} \quad x = \begin{bmatrix} a \\ b \\ c \end{bmatrix} \quad b = \begin{bmatrix} 0 \\ 0 \\ 1 \end{bmatrix}$$

Since $\pi_i = \alpha^a \rho^b m^c$

and $t = \pi_i$ (constant).

Solve using Matlab or linear algebra for:

$$X = \begin{bmatrix} -1 \\ -2/3 \\ 2/3 \end{bmatrix}, \quad \pi_i = \frac{m^{2/3}}{\alpha \cdot \rho^{2/3}} \text{ (constant)}$$

But α and ρ are (presumably) constant for all turkeys. So:

$$t = C_1 m^{2/3}$$

From the web, we can find a table of empirical data of cooking time vs. turkey mass.

Plot t vs. $m^{2/3}$, and solve using linear least-squares regression for the trend line. Then:

$$t = 0.864 \left(m^{2/3} \right) \quad (\text{Results may vary})$$

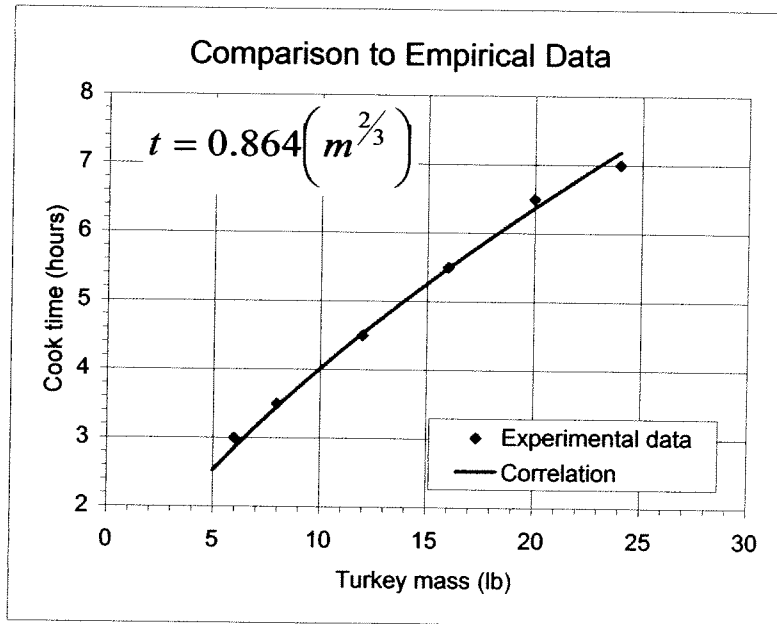
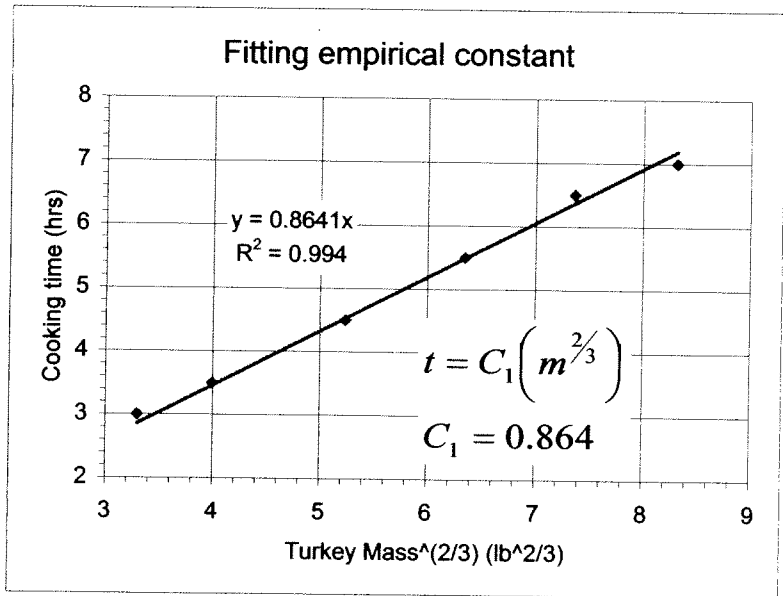
HW#7 Problem #1

Experimental data

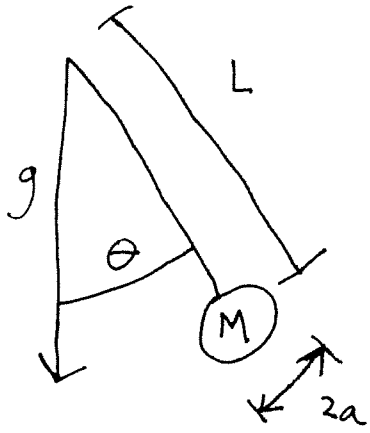
Mass (lbm)	Cooking time (hr)	weight ^{2/3}
6	3	3.30
8	3.5	4.00
12	4.5	5.24
16	5.5	6.35
20	6.5	7.37
24	7	8.32

Correlation: $t = 0.864 \left(m^{2/3} \right)$

Mass (lbm)	Correlated time (hr)
5	2.53
6	2.85
7	3.16
8	3.46
9	3.74
10	4.01
11	4.27
12	4.53
13	4.78
14	5.02
15	5.26
16	5.49
17	5.71
18	5.93
19	6.15
20	6.37
21	6.58
22	6.78
23	6.99
24	7.19



2. Damped pendulum in a viscous fluid



$$ML \frac{d^2 \theta}{dt^2} = -Mg \sin(\theta) - 6\pi\mu a L \frac{d\theta}{dt}$$

$$\theta \Big|_{t=0} = \theta_0 ; \quad \frac{d\theta}{dt} \Big|_{t=0} = 0$$

Start by rendering the equation dimensionless.

$$t^* = \sqrt{\frac{g}{L}} t, \quad \theta^* = \frac{\theta}{\theta_0}$$

Note: θ is already dimensionless, but θ^* ranges from $[0, 1]$.

$$Mg \theta_0 \frac{d^2 \theta^*}{dt^{*2}} = -Mg \sin(\theta^* \theta_0) - 6\pi\mu a \theta_0 \sqrt{gL} \frac{d\theta^*}{dt^*}$$

divide through by $Mg \theta_0$

$$\frac{d^2 \theta^*}{dt^{*2}} + \frac{\sin(\theta^* \theta_0)}{\theta_0} + \frac{6\pi\mu a \sqrt{gL}}{Mg} \frac{d\theta^*}{dt^*} = 0$$

two dimensionless groups are:

$$\pi_1 = \frac{6\pi\mu a \sqrt{gL}}{Mg} = \boxed{\frac{6\pi\mu a}{M} \sqrt{\frac{L}{g}}} \rightarrow \text{damping coefficient}$$

$$\pi_2 = \boxed{\theta_0} \rightarrow \text{initial angle} \quad \Rightarrow$$

(a)

2. Continued

Physical meanings:

damping coefficient: describes the drag on the sphere. If $\pi_1 \rightarrow 0$, the pendulum will oscillate infinitely. If $\pi_1 \rightarrow$ large, the pendulum will settle very slowly.

At critical damping, $\pi_1 = 1$. This corresponds to the pendulum just settling to $\theta = 0$ with no oscillations, but without overdamping.

initial angle: self-explanatory.

(b) At critical damping:

$$\frac{6\pi\mu a}{M} \sqrt{\frac{L}{g}} = 1 \quad \Rightarrow \quad \boxed{\mu_{\text{critical}} = \frac{M}{6\pi a} \sqrt{\frac{g}{L}}}$$

To estimate the time to reach 25%, just use the time scaling.

$$\boxed{t_{25\%} = \sqrt{\frac{L}{g}}}$$



2. continued

(c) Make the approximation given; that
 $\sin(\theta^* \theta_0) = \theta^* \theta_0$ when $\theta^* \theta_0$ is small.

This gives:

$$\frac{d^2 \theta^*}{dt^{*2}} + \frac{6\mu\pi a}{M} \sqrt{\frac{L}{g}} \frac{d\theta^*}{dt^*} + \theta^* = 0$$

With B.C.:

$$\theta^* \Big|_{t^*=0} = 1 \quad \frac{d\theta^*}{dt^*} \Big|_{t^*=0} = 0$$

The characteristic equation is of the form:

$$a\theta^{*r} + b\theta^{*r'} + c\theta^* = 0$$

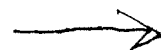
With eigenvalues:

$$\lambda_{1,2} = \frac{-b \pm \sqrt{b^2 - 4ac}}{2a}$$

Recall from differential equations that critical damping occurs when $\lambda_1 = \lambda_2$, or when $\sqrt{b^2 - 4ac} = 0$.

So:

$$\sqrt{\left(\frac{6\pi\mu a}{M} \sqrt{\frac{L}{g}}\right)^2 - 4} = 0, \Rightarrow \boxed{\mu_{\text{critical}} = \frac{2M}{6\pi a} \sqrt{\frac{g}{L}}}$$



2. Continued

If we substitute this into the equation,

$$\theta^{*''} + 2\theta^{*'} + \theta^* = 0$$

and $\lambda = -1$.

Solution:

$$\theta^* = (C_1 + C_2 t^*) e^{\lambda t^*}$$

with boundary conditions:

$$\theta^* \Big|_{t^*=0} = 1 \quad \Rightarrow \quad C_1 = 1$$

$$\frac{d\theta^*}{dt^*} \Big|_{t^*=0} = 0 \quad \Rightarrow \quad \frac{d\theta^*}{dt^*} \Big|_{t^*=0} = \left[C_1 \lambda e^{\lambda t^*} + C_2 e^{\lambda t^*} + C_2 \lambda t^* e^{\lambda t^*} \right]_{t^*=0}$$

$$0 = \lambda + C_2 \Rightarrow C_2 = -\lambda$$

$$\text{So: } \theta^* = (1 + t^*) e^{-t^*}$$

Now find t^* for when $\theta^* = 0.25$

$$0.25 = (1 + t^*) e^{-t^*} \quad \Rightarrow \quad t^* = \overset{2.69}{\cancel{2.69}}$$

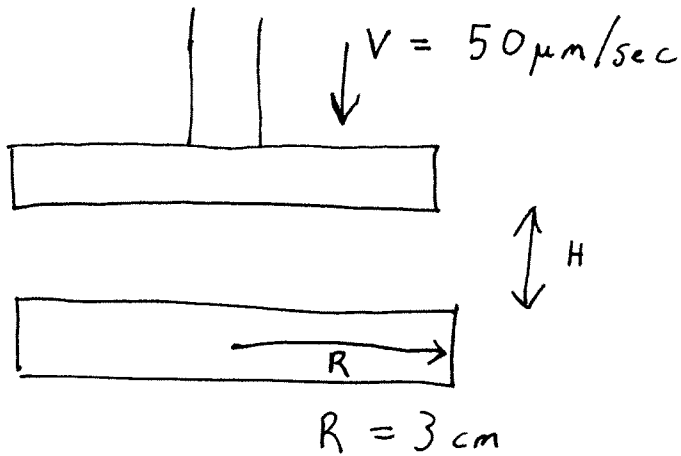
Compare:

	<u>Dimensional Analysis</u>	<u>Exact</u>
$t_{25\%}$	$\sqrt{\frac{L}{g}}$	$\overset{2.69}{\cancel{2.69}} \sqrt{\frac{L}{g}}$
μ_{critical}	$\frac{M}{6\pi a} \sqrt{\frac{g}{L}}$	$\frac{2M}{6\pi a} \sqrt{\frac{g}{L}}$

$$\Rightarrow t_{25\%} = \overset{2.69}{\cancel{2.69}} \sqrt{\frac{L}{g}}$$

Note: both μ_{critical} and $t_{25\%}$ were under-predicted by dim

3. Parallel-plate Viscometer



$$F = 10^4 \text{ dynes}$$

$$\mu_{\text{air}} = 1.8 \times 10^{-4} \text{ poise}$$

(a) Find the error in the gap set zero.

- This is the height H when the force $F = 10^4$ dynes, for the given V and μ . (and R)

Start with the continuity equation in cylindrical coordinates.

$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial}{\partial r} (\rho r v_r) + \frac{1}{r} \frac{\partial}{\partial \theta} (\rho v_\theta) + \frac{\partial}{\partial z} (\rho v_z) = 0$$

$$\frac{1}{r} \frac{\partial}{\partial r} (r v_r) + \frac{\partial}{\partial z} (v_z) = 0$$

Non-dimensionalize:

$$v_z^* = \frac{v_z}{V} \quad v_r^* = \frac{v_r}{U} \quad r^* = \frac{r}{R} \quad z^* = \frac{z}{H}$$

$$\frac{U}{R} \frac{1}{r^*} \frac{\partial}{\partial r^*} (r^* v_r^*) + \frac{V}{H} \frac{\partial v_z^*}{\partial z^*} = 0$$

divide through by $\frac{U}{R}$, find the dimensionless group $\frac{VR}{UH}$

$$\text{So } U = \frac{R}{H} V$$



3. continued

Since $\frac{R}{H}$ is small, $U \ll V$, and we can assume

quasi-parallel flow in r -direction.

Now look at the r -momentum equation:

$$\rho \left(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta^2}{r} + v_z \frac{\partial v_r}{\partial z} \right) = -\frac{\partial p}{\partial r} +$$

$$+ \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} (r v_r) \right) + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial^2 v_r}{\partial z^2} \right] + \rho g_r$$

Use the non-dimensional substitutions: $t^* = \frac{V}{H} t$ $P^* = \frac{P - P_0}{\Delta P_c}$

$$\rho \frac{U^2}{R} \left(\frac{\partial v_r^*}{\partial t^*} + v_r^* \frac{\partial v_r^*}{\partial r^*} + v_z^* \frac{\partial v_r^*}{\partial z^*} \right) = -\frac{\Delta P_c}{R} \frac{\partial P^*}{\partial r^*} +$$

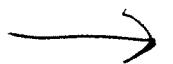
$$+ \mu \frac{U}{H^2} \left[\frac{H^2}{R^2} \frac{\partial}{\partial r^*} \left(\frac{1}{r^*} \frac{\partial}{\partial r^*} (r^* v_r^*) \right) + \frac{\partial^2 v_r^*}{\partial z^{*2}} \right]$$

Since Re is low, use the viscous scaling. divide by $\mu \frac{U}{H^2}$:

$$\left(\frac{\rho U H}{\mu} \right) \left(\frac{\partial v_r^*}{\partial t^*} + v_r^* \frac{\partial v_r^*}{\partial r^*} + v_z^* \frac{\partial v_r^*}{\partial z^*} \right) = - \left(\frac{\Delta P_c H^2}{R \mu U} \right) \frac{\partial P^*}{\partial r^*} +$$

$$+ \frac{H^2}{R^2} \frac{\partial}{\partial r^*} \left(\frac{1}{r^*} \frac{\partial}{\partial r^*} (r^* v_r^*) \right) + \frac{\partial^2 v_r^*}{\partial z^{*2}}$$

We can set $\frac{\Delta P_c H^2}{R \mu U} = 1$, so $\Delta P_c = \frac{R \mu U}{H^2}$



3. continued

Since $H \ll R$, and Re is low, we can reduce the equation to:

$$\frac{\partial P^*}{\partial r^*} = \frac{\partial^2 V_r^*}{\partial z^{*2}}$$

Assuming pressure gradient is constant, we can integrate twice to get:

$$V_r^* = \frac{1}{2} \frac{\partial P^*}{\partial r^*} z^{*2} + C_1 z^* + C_2$$

Apply B.C.

$$V_r^* \Big|_{z^*=0} = 0 \Rightarrow C_2 = 0$$

$$V_r^* \Big|_{z^*=1} = 0 \Rightarrow C_1 = -\frac{1}{2} \frac{\partial P^*}{\partial r^*}$$

$$\text{So } \underline{V_r^* = -\frac{1}{2} \frac{\partial P^*}{\partial r^*} z^* (1-z^*)}$$

Now we can use a mass balance to find $\frac{\partial P^*}{\partial r^*}$

Mass in = mass out

$$V \pi r^{*2} R^2 = U H R 2 \pi r^* \int_0^1 V_r^* dz^*$$

$$\frac{1}{2} r^* = \int_0^1 V_r^* dz^*$$

and since

$$U = \frac{R}{H} V$$



3. Continued

$$\int_0^1 -\frac{1}{2} \frac{\partial P^*}{\partial r^*} (z^* - z^{*2}) dz^* = -\frac{1}{2} \frac{\partial P^*}{\partial r^*} \left(\frac{z^{*2}}{2} \Big|_0^1 - \frac{z^{*3}}{3} \Big|_0^1 \right)$$

$$\frac{1}{2} r^* = -\frac{1}{2} \frac{\partial P^*}{\partial r^*} \frac{1}{6}$$

$$\text{So: } \frac{\partial P^*}{\partial r^*} = -6 r^*$$

Boundary condition: $P^* \Big|_{r^*=1} = 0$

$$P^* = 3(1 - r^{*2})$$

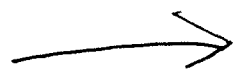
From physics,

$$F = \int_0^R P 2\pi r dr = \Delta P_c R^2 2\pi \int_0^1 P^* r^* dr^*$$

Substitute in our expression for pressure:

$$F = 6\pi \Delta P_c R^3 \int_0^1 r^* - r^{*3} dr^* = \frac{6}{4} \pi \Delta P_c R^3 = \frac{3}{2} \pi \left[\frac{R \mu U}{H^2} \right] R^3$$

$$\text{So } \boxed{F = \frac{3\pi R^4 \mu U}{2H^3}}$$



3. Continued

(a) what is the error in the gap set?

Solve for

$$H = \left(\frac{3 \pi R^4 \mu V}{2 F} \right)^{1/3} = \left(\frac{3 \pi (3 \text{ cm})^4 (1.8 \times 10^{-4} \frac{\text{g}}{\text{cm} \cdot \text{s}}) (50 \times 10^{-4} \frac{\text{cm}}{\text{sec}})}{2 (10^4 \frac{\text{g} \cdot \text{cm}}{\text{s}^2})} \right)^{1/3}$$

$$H = 0.00325 \text{ cm}$$

$$H = 32.5 \mu\text{m} = \text{error}$$

(b)

in order to reduce this to $3.25 \mu\text{m}$,

V must be:

$$V = \frac{F 2 H^3}{3 \pi R^4 \mu} = 0.05 \mu\text{m}/\text{sec}, = 50 \text{ nm}/\text{sec}$$

This is WAY too slow. Not practical.

(c) if $H_{\text{actual}} = 232.5 \mu\text{m}$

$H = 200 \mu\text{m}$, what is the error in viscosity?

from Problem Set 6,

$$T = \frac{-\pi \mu \Omega R^4}{2 H}, \text{ so } \mu = H \left[\frac{2 T}{\pi \Omega R^4} \right]$$

$$\frac{\mu_{\text{exp}}}{\mu} = 1.16$$

$$\text{thus, } \frac{\mu_{\text{exp}}}{\mu} = \frac{232.5}{200} = 1.16$$

4. Prove that $\nabla^2 p = 0$ for an incompressible fluid at $Re = 0$.

N-S equation:

$$\rho \left(\frac{\partial \underline{u}}{\partial t} + \underline{u} \cdot \nabla \underline{u} \right) = -\nabla P + \mu \nabla^2 \underline{u} + \rho \underline{g}$$

Index notation:

$$\rho \left(\frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} \right) = -\frac{\partial P}{\partial x_i} + \mu \frac{\partial^2 u_i}{\partial x_j^2} + \rho g_i$$

Non-dimensionalize

$$u_i^* = \frac{u_i}{V} \quad x_i^* = \frac{x_i}{L} \quad g_i^* = \frac{g_i}{g} \quad P^* = \frac{P - P_0}{(\mu V / L)} \quad t^* = \frac{t}{(L/V)}$$

Then:

$$\rho \frac{V^2}{L} \left[\frac{\partial u_i^*}{\partial t^*} + u_j^* \frac{\partial u_i^*}{\partial x_j^*} \right] = -\frac{\mu V}{L^2} \frac{\partial P^*}{\partial x_i^*} + \frac{\mu V}{L^2} \frac{\partial^2 u_i^*}{\partial x_j^{*2}} + g \rho g_i^*$$

We know $Re \rightarrow 0$, so we use the viscous scaling.

Divide through by $\mu \frac{V}{L^2}$:

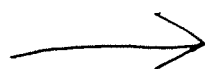
$$\frac{\rho V L}{\mu} \left[\frac{\partial u_i^*}{\partial t^*} + u_j^* \frac{\partial u_i^*}{\partial x_j^*} \right] = -\frac{\partial P^*}{\partial x_i^*} + \frac{\partial^2 u_i^*}{\partial x_j^{*2}} + \underbrace{\left(\frac{\rho g L^2}{\mu V} \right)}_{\frac{Re}{Fr}} g_i^*$$

Re

Fr

And with $Re \rightarrow 0$,

$$\frac{\partial^2 u_i^*}{\partial x_j^{*2}} = \frac{\partial P^*}{\partial x_i^*}$$



4. Continued

Now take the divergence. The ODE is:

$$\frac{\partial^2 u_i^*}{\partial x_j^{*2}} = \frac{\partial p^*}{\partial x_i^*}$$

or $\nabla^{*2} \underline{u}^* = \underline{\nabla}^* p$ in Gauss.

Divergence:

$$\frac{\partial}{\partial x_i^*} \frac{\partial^2 u_i^*}{\partial x_j^{*2}} = \frac{\partial}{\partial x_i^*} \frac{\partial p^*}{\partial x_i^*}$$

or $\underline{\nabla}^* \cdot \nabla^{*2} \underline{u}^* = \underline{\nabla}^* \cdot \underline{\nabla}^* p$ in Gauss.

Note that $\underline{\nabla}^*$ and ∇^{*2} commute. ~~So~~ so:

$$\frac{\partial^2}{\partial x_j^{*2}} \frac{\partial u_i^*}{\partial x_i^*} = \frac{\partial^2 p^*}{\partial x_i^{*2}}$$

or $\nabla^{*2} (\underline{\nabla}^* \cdot \underline{u}) = \nabla^{*2} p$ in Gauss.

We know from continuity that $\frac{\partial u_i^*}{\partial x_i^*} = 0$, or $\underline{\nabla} \cdot \underline{u} = 0$,

So:

$$\boxed{\frac{\partial^2 p^*}{\partial x_i^{*2}} = 0}$$

or $\boxed{\nabla^{*2} p = 0}$