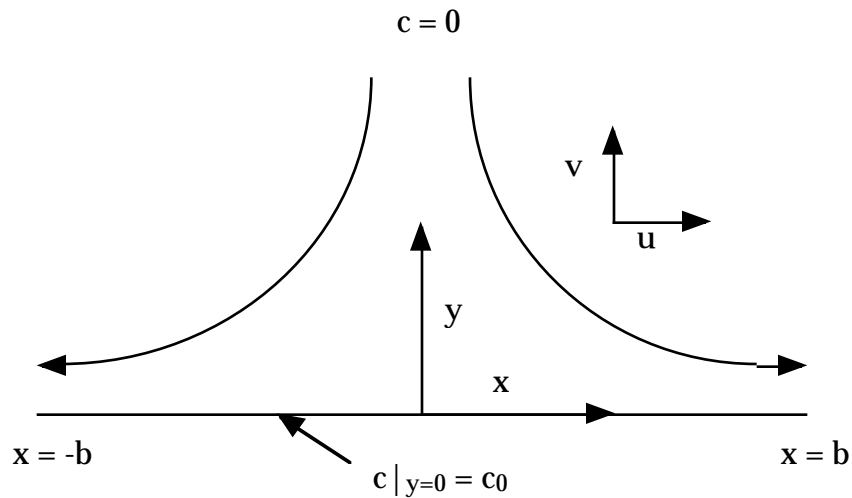


**CHEG 355 Transport Phenomena I  
Final Exam**

**December 12, 2005**

**Closed Books and Notes**

Problem 1. (30 points) Scaling analysis of boundary layer flows. An important problem in mass transfer is the rate of diffusion of a solute from a planar surface in the presence of a stagnation flow. Consider the two-dimensional problem depicted below. A planar jet impinges on a plate of width  $2b$ .



a. Very close to the surface the velocity profile is known exactly: for a viscous flow the velocity in the  $x$ -direction is given by  $u = Axy$ , with a corresponding (non-zero!) velocity in the  $y$ -direction. Using the continuity equation and the condition that  $v$  vanishes at the plate, determine  $v$ .

b. The concentration distribution is given by the convective diffusion equation (both  $u$  and  $v$  are non-zero!). Scaling this equation, determine the conditions under which we would get a boundary-layer problem for mass transfer (e.g., under which we can ignore diffusion in the  $x$ -direction), and the characteristic boundary layer thickness.

$$\underline{u} \cdot \underline{\nabla} c = D \nabla^2 c$$

c. If the mass flux at the surface is given by:

$$N \Big|_{y=0} = -D \frac{\partial c}{\partial y} \Big|_{y=0}$$

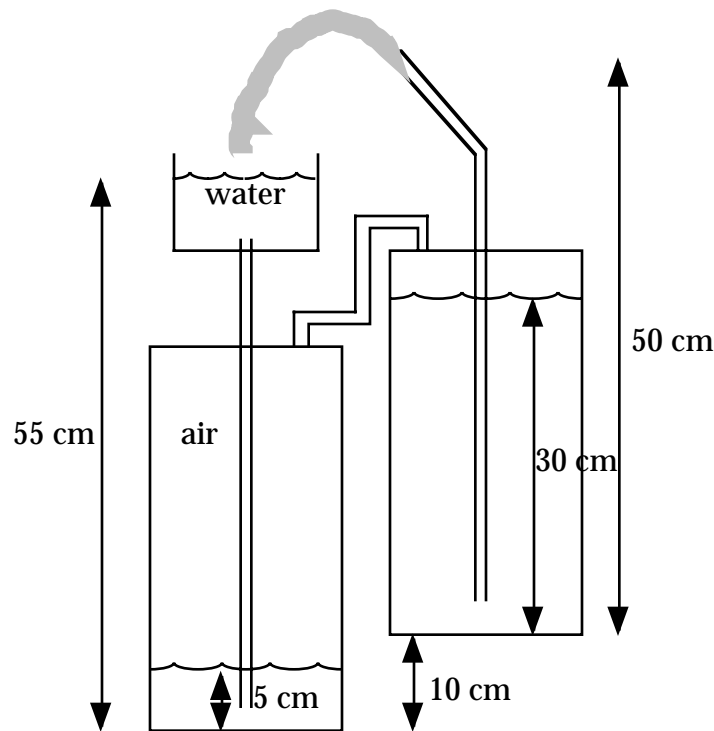
determine via scaling analysis how the total rate of mass transfer from a plate of width  $2b$  in the  $x$  direction and  $W$  in the third direction (e.g., into the paper, the direction that doesn't matter) scales with the parameters in the problem.

d. Using simple affine stretching, show that the problem admits a self-similar solution. Solve the resulting ODE for the concentration distribution. You may leave your final answer in terms of an integral.

Problem 2. (20 points) Hero's Fountain. In class we demonstrated Hero's Fountain, attributed to Hero of Alexandria a couple of millenia ago. In this problem we analyze its performance.

a). Neglecting all frictional losses, what is the exit velocity and flow rate of the fountain? All pipes are 0.5cm ID smooth tubes.

b). Modify your answer by accounting for the head losses in the pipes and fittings. Correlations for friction factors in pipes and fittings are given below. You may take the total length of pipe to be 100 cm. You will probably need to do a couple of iterations to get the friction factor right.



$$h_L = \frac{\langle u \rangle^2}{2g} \sum K + 4 f_f \frac{L}{D} \frac{\langle u \rangle^2}{2g}$$

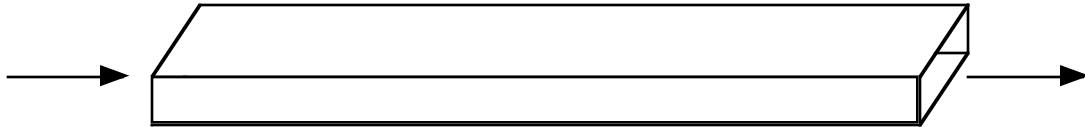
$$f_f = \frac{16}{Re} ; Re < 2100$$

$$f_f \approx \frac{0.0791}{Re^{1/4}} ; 3000 < Re < 10^5$$

$$\frac{1}{\sqrt{f_f}} = 4.0 \log_{10} \left( Re \sqrt{f_f} \right) - 0.40 ; Re > 3000$$

Fitting	K value
sudden contraction	0.45
sudden expansion	1.0
45° elbow	0.35

Problem 3). (20 points) Plane Poiseuille Flow: A problem which is currently being investigated in bioengineering laboratories is the phenomenon of cell adhesion to surfaces in the presence of hydrodynamic stresses. This is very important in the design of biocompatible materials, for example. To study this, a researcher has built a rectangular flow cell which is  $100\mu\text{m}$  deep,  $2\text{mm}$  wide, and  $2\text{cm}$  long. The objective is to have a wall shear stress (e.g., stress at the lower wall - the  $2\text{mm} \times 2\text{cm}$  surface - where cell adhesion is being studied) of  $100\text{ dyne}/\text{cm}^2$ . If the working fluid has the same viscosity as water, what should the flow rate of the pump supplying the fluid be? Make any simplifications you need to, but provide a **brief** justification.



Problem 4. (30 points) Pump Curves / Additional Readings / Short Answer:

The first five questions refer to the pump curve on the last page:

1. It is desired to pump  $60\text{ liters}/\text{sec}$  from a pond to an elevation of  $30\text{ meters}$ . If we neglect all frictional losses (say we use a really fat pipe!) is the pump CP200 recommended for the job?
2. What is the RPM required to do the job?
3. What is the work done by the pump on the fluid per unit time?
4. What is the efficiency of the pump at the operating conditions?
5. How far up the hill from the level of the pond can we put the pump? (Again, neglect frictional losses) (Note:  $1\text{atm} \approx 10.3\text{ m water}$ )
6. In our class demonstration, when we allowed a rod to settle in a viscous liquid ( $Re = 0$ ), we observed that it didn't rotate. If inertial effects are important, it does. Why is the behavior different in this case?
7. For a shear stress of  $100\text{ dynes}/\text{cm}^2$  in the turbulent flow of water through a pipe, about how rough does the pipe wall have to be before it influences the flow?
8. At high  $Re$ , drag principally results from:
 

A. Potential Flow	B. Boundary Layer Separation
C. Skin Friction	D. Turbulence
9. Ensuring that the NPSHR is met for a pump installation will help prevent:
 

A. Cavitation in the pump	B. Damage to pipes and fittings due to vibrations
C. Reduced pump performance	D. All of the above

10. The displacement thickness is defined as:

$$\delta^* = \int_0^{\infty} \left( 1 - \frac{u}{U} \right) dy$$

Provide a brief physical interpretation of this quantity.

11. Just as in the case of turbulent momentum transfer where we define a turbulent kinematic viscosity  $\nu_t$ , so in the case of turbulent energy transfer we can define a turbulent thermal diffusivity  $\alpha_t$ . The turbulent Prandtl number is the ratio of these quantities ( $Pr_t = \nu_t / \alpha_t$ ). What is its approximate magnitude and why?

12. Experimentally, how can you most accurately calculate the shear stress on a plate in boundary layer flow at high Reynolds numbers from the velocity profile?

13. Give a physical description of the Reynolds stress (e.g., where does it come from?).

14. Using index notation, write down the force exerted by the surrounding fluid on an arbitrary object in terms of the stress tensor  $\sigma_{ij}$ .

15. Briefly describe one method for preventing stall on an aircraft wing.

# SYKES PUMPS

CURVE: CP2000108 ISSUE 3  
DATE OF ISSUE: 9 AUGUST 2002

PUMP : CP-200

SUCTION 200mm	DISCHARGE 200mm	MAX. SPHERE 80mm	IMPELLER 3 VANE	IMPELLER ø295mm	IMPELLER & WEAR PLATES 316 5/5
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